

## TEMPERATURE PROGRAMMED DESORPTION OF AMMONIA FROM DEALUMINATED CLINOPTILOLITE

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Received 25. 11. 1992

*Ammonia was used for adsorption on calcined dealuminated NH-clinoptilolite. Four acid site types of clinoptilolite were determined by TPD. Extraframework aluminium remained in clinoptilolite structure after dealumination increases the relative number of weak acid sites and has blocking influence on strong acid sites determination.*

*Key words: clinoptilolite, dealuminated, TPD, DTG, mass spectra*

## INTRODUCTION

Temperature programmed desorption of probe molecules is, beside of IR spectroscopy, <sup>1</sup>H-MAS-NMR and microcalorimetry a method frequently used for characterization of acid properties of zeolites.

Hegde et al. [1] studied the acidity of zeolite Beta by TPD of ammonia. Only desorption peak in the 653–673 K region was found to correlate with the Al content, acidity and catalytic activity of zeolite. The peak at 823 K is due to dehydroxylation, because no NH<sub>3</sub> was detected in the desorbate, only H<sub>2</sub>O was observed.

Lok et al. [2] reported the TPD spectra for ammonia desorption from zeolites Y and L. NH<sub>4</sub>-Y exhibited three desorption peaks at 393, 489 and 553 K. Si-enriched NH<sub>4</sub>-Y showed two not well resolved NH<sub>3</sub> peaks at 586 and 705 K. The NH<sub>3</sub>-TPD of NH<sub>4</sub>-L sample showed 3 peaks at 385, 691 and 821 K. The last peak being associated with partial decomposition of the crystal.

Meyers et al. [3] studied the acidity changes of mordenite using TPD-NH<sub>3</sub> methods. The high-temperature peak at 475°C depended on structural aluminium content in mordenite. The amount of NH<sub>3</sub> desorbed at high temperature was taken as a measure of strong acidity.

Auroux et al. [4] combined the TPD and comparative calorimetric studies of H-ZSM5, H-Y and H-Ferrierite for acid sites distribution determination. The weight loss and ΔH of NH<sub>3</sub> desorption was measured at increasing temperature. Three different acid sites were found in all cases, but the peak temperatures and amount of desorbed NH<sub>3</sub> varied at high-temperature peaks from 560 to 720°C and from 138 to 165 KJ/mol, respectively.

The aim of present work is to compare the relative acid sites number of natural cation-, NH<sub>4</sub>-, dealuminated- and acid washed dealuminated-forms of clinoptilolite and follow up the influence of dealumination degree for single peaks position shift.

## EXPERIMENTAL

## Material

Rhyolite tuff containing 70 mass % of clinoptilolite was used as a starting material. The sample was treated with 3M NH<sub>4</sub>Cl at room temperature and during 3 times 24 hours. Dealumination was carried out by stirring of NH<sub>4</sub>-clinoptilolite with 0.75M (NH<sub>4</sub>)<sub>2</sub>SiF<sub>6</sub> at 95°C during 1, 3, 16 and 24 hours. Samples D, D<sub>0</sub>, D<sub>1</sub>, D<sub>3</sub>, D<sub>6</sub> and D<sub>11</sub> (Table I) were deammoniated and dehydrated at 500°C, in dynamic vacuum (5 Pa) for 5 hours. The probe molecules were sorbed after cooling for 1 hour at 50°C. Then the samples were outgassed at 200°C 1 hour to remove physically sorbed probe molecules and studied at thermal analysis.

## Acid washing

Dealuminated samples were washed with 1 N HCl at room temperature during 1.5 hour, to remove extraframework (EFA1). The method of acid washing was chosen on the base of condition, that the aluminium loss during the acid treatment must be lower than 5 mass % in the case of starting material.

## Probe molecule

NH<sub>3</sub> – liquid NH<sub>3</sub> was saturated by dried KSCN. Trace amount of water was removed by NaA zeolite and the solution was used for sorption at 22±2°C and at the saturated steam pressure.

## Methods

Derivatograph Q-1500 (MOM Budapest) was used for DTA, DTG and TG measurements. 560 mg of sample was analysed in air and N<sub>2</sub> at heating rate 20 K/min. DTG curves were fitted using Pitha & Jones computer program [5] for fitting curves to infrared

Table 1  
Characterization of the dealuminated samples

Sample	Reaction time [h]	Composition	Si/Al ratio
D	0	$\text{Ca}_{2.0}\text{Mg}_{0.1}\text{Na}_{0.6}\text{K}_{1.9}\text{Al}_{6.7}\text{Si}_{29.3}\text{O}_{72}$	4.37
D <sub>0</sub>	0	$(\text{NH}_4)_{6.7}\text{Al}_{6.7}\text{Si}_{29.3}\text{O}_{72}$	4.37
D <sub>1</sub>	1	$(\text{NH}_4)_{6.03}\text{Al}_{6.03}\text{Si}_{29.97}\text{O}_{72}$	4.97
D <sub>3</sub>	3	$(\text{NH}_4)_{5.26}\text{Al}_{5.26}\text{Si}_{30.74}\text{O}_{72}$	5.84
D <sub>6</sub>	16	$(\text{NH}_4)_{4.21}\text{Al}_{4.21}\text{Si}_{31.79}\text{O}_{72}$	7.55
D <sub>11</sub>	24	$(\text{NH}_4)_{4.15}\text{Al}_{4.15}\text{Si}_{31.85}\text{O}_{72}$	7.67

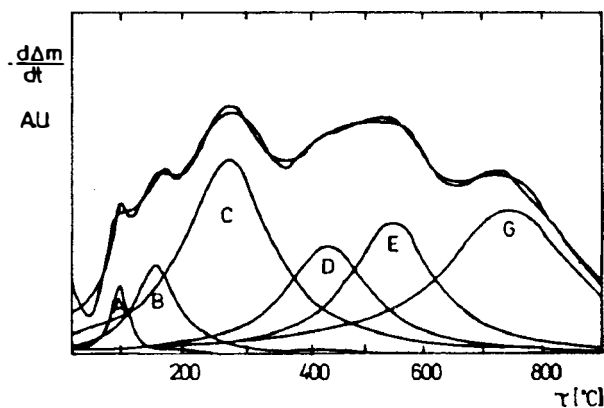


Fig. 1. DTG curve of  $\text{NH}_3$  desorption from  $D_3$  sample and fitted desorption peaks.

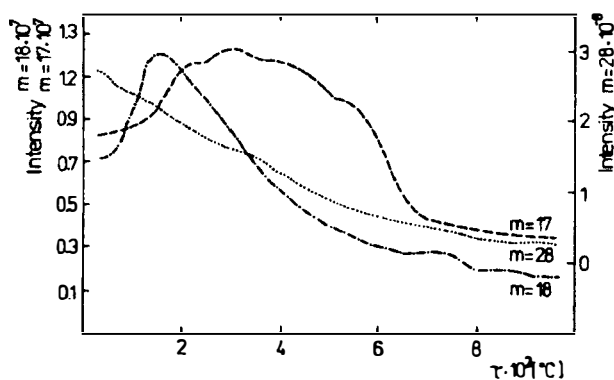


Fig. 2. Mass spectrum of  $\text{NH}_3$  desorption from  $D_3$  sample.

band envelope. The relative peak areas were calculated taking into account B-, C-, D- and E- $\text{NH}_3$  peaks (Fig. 1).

Netzsch STA-QMS, system 409 thermal analyser was used for desorption products analysis. Heating

rate 10 K/min and flow rate of Ar 80 ml/min were used.

The possibility of DTG and mass spectra comparing was checked by means of comparison  $\text{NH}_3$  desorption from clinoptilolite at the atmosphere of air and  $\text{N}_2$  (Fig. 5). The slight shift of DTG and DTA peaks to higher temperature was found in the case of  $\text{N}_2$  (flow rate of  $\text{N}_2$  was 80 ml/min.).

#### RESULTS AND DISCUSSION

DTG curves of  $\text{NH}_3$  desorption from starting cation-, NH- and dealuminated-forms of clinoptilolite are in Fig. 4. The shape changes of desorption curves describe the changes of clinoptilolite acid properties after decationization and dealumination.

Six desorption peaks were fitted in DTG curves of  $\text{NH}_3$  desorption. Using program for optimization of temperatures, intensities and half-width it was achieved good agreement summary envelope function with experimental DTG curve (Fig. 1).

Desorption peak A- $\text{NH}_3$  (Fig. 1) occurs at 160°C ( $D_0$ ). The higher content of  $\text{NH}_3$  ( $m=17$ ) ( $m$  = molecular weight) along with water ( $m=18$ ) was observed in the case of  $\text{NH}_3$  desorption (Fig. 2). Curve  $m=28$  was scanned in order to check the possibility of desorbed  $\text{NH}_3$  oxidation connected with  $\text{N}_2$  formation. The overlapping of  $m=18$  and  $m=17$  curves (Fig. 2) was found below the evacuation temperature (200°C). This phenomenon indicates the possibility of small  $\text{NH}_3$  molecules migration in the zeolite porous structure. From present measurement can not be judged the influence of adsorbed water molecules on the  $\text{NH}_3$  migration degree in the structure. The desorption maxima of A- $\text{NH}_3$  were shifted from 160 ( $D_0$ ) to 208°C ( $D_{11}$ ) with dealumination. The shape similarity of D and  $D_{11}$  curves (Fig. 4) can be explained by the same influence of the EFA1 and exchangeable starting cations on the water adsorption.

The position of desorption peak B- $\text{NH}_3$  is at 245°C ( $D_0$ ) (Fig. 1). The position change of B-peak with

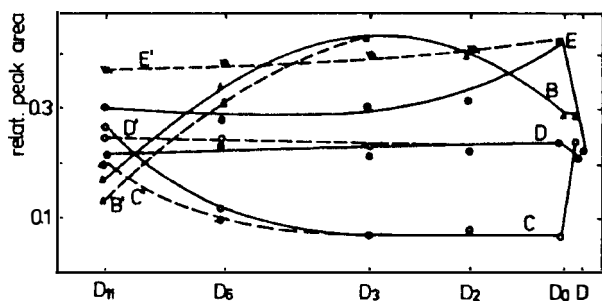


Fig. 3. Dependence of relative peak areas of ammonia desorption on dealumination degree.

dealumination is slightly shifted to higher temperatures. The course of  $m=18$  and  $m=17$  curves (Fig. 2) indicate the presence of  $\text{NH}_3$  and small amount of water at desorption products. Water content at desorption gases is due to moisture adsorption on very weak and unoccupied acid sites and supposed migration of  $\text{NH}_3$  and water in zeolite structure. B- $\text{NH}_3$  curve (Fig. 3) shows the dependence of peak B- $\text{NH}_3$  area from aluminium content. The desorbed amount of  $\text{NH}_3$  exhibits maximum in  $D_3$  sample. Supposing, that the peak area corresponds to number of acid sites, the relative number of weak acid centers B- $\text{NH}_3$  coincides with the shape of curve B (Fig. 3). The relative number of acid sites B- $\text{NH}_3$  decreases in accordance with B'- $\text{NH}_3$  curve after acid washing. EFA1, retaining at dealuminated samples after washing, is removed by acid treatment. Molecules of ammonia can be bonded onto EFA1 because of small kinetic diameter (0.26 nm) and can be bonded at the porous system, partially occupied by EFA1.

The peak positions of C- $\text{NH}_3$  (Fig. 1) were shifted from 370 ( $D_0$ ) to 350°C ( $D_{11}$ ) at dealumination. Peak temperature decreasing is connected with partial pore system destruction and mesopore formation. The relative mesopore volume increases with dealumination (6) and the diffusion of probe molecules is easier. The relative number of acid sites C- $\text{NH}_3$  (Fig. 3) increases after dealumination. The number of acid sites after acid washing is evident from C'- $\text{NH}_3$  curve (Fig. 3). We described previously (7) the faster weak acid sites decreasing in comparison with strong acid sites. The C-C' curves for  $\text{NH}_3$  refer to probe molecules adsorption on EFA1, the certain amount of which was not removed by acid washing and remained in clinoptilolite structure.

Peak position of D- $\text{NH}_3$  (Fig. 1) is at 480°C ( $D_0$ ). The shift of peak temperature was found to 448°C ( $D_{11}$ ) at dealumination. In D- $\text{NH}_3$  desorption gaseous products was only  $\text{NH}_3$  detected (Fig. 2). Relative peak area of D- $\text{NH}_3$  (Fig. 3) slightly decreases after dealumination. The number of acid sites slightly in-

creases after acid treatment (Fig. 3). This indicates the blocking influence of EFA1, removable by HCl treatment, for  $\text{NH}_3$  adsorption.

Peak E- $\text{NH}_3$  (Fig. 1) has desorption maximum at temperature interval from 593 ( $D_0$ ) to 569°C ( $D_{11}$ ). At desorption gaseous products at temperature interval of E- $\text{NH}_3$  (Fig. 1) was identified only ammonia (Fig. 2). Relative area of desorption peaks E corresponding with relative number of strong acid sites

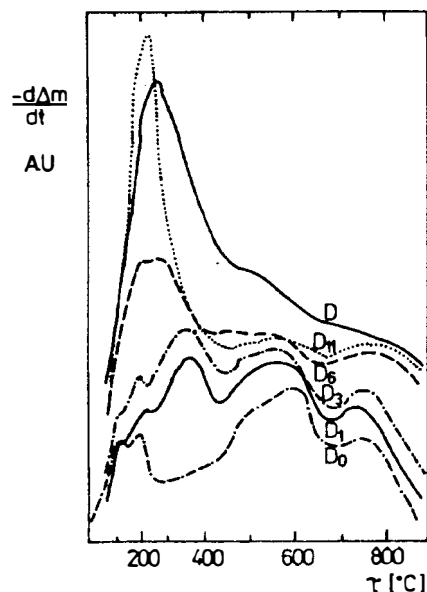


Fig. 4. DTG curves of ammonia desorption for various dealumination degree.

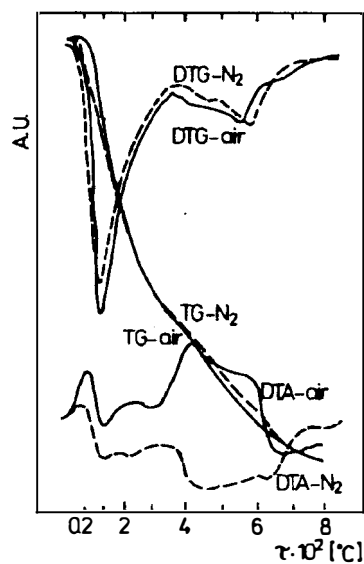


Fig. 5. The comparison of thermal analysis results of  $\text{NH}_3$ - $D_0$  sample carried in air and  $\text{N}_2$ .

decreases with dealumination. the significant increasing of amount of desorbed  $\text{NH}_3$  was found after acid treatment of dealuminated samples ( $\text{E}^1\text{-NH}_3$ ) in comparison with  $\text{E-NH}_3$ . The significant influence of acid treatment of dealuminated clinoptilolite can be supposed as a result of accession improving of strong acid centers for sorption of ammonia molecules.

Desorption peaks  $\text{G-NH}_3$  (Fig. 1) present the weight loss connected with dehydroxylation of Bronsted acid sites and formation of Lewis acid ones. The presence of water can be found at  $730^\circ\text{C}$  (Fig. 2) at desorption products.

$\text{NH}_3$  seems convenient for clinoptilolite acid sites determination because of small kinetic diameter (0.26nm) and desorption without decomposition. there is the possibility of partial  $\text{NH}_3$  molecules redistribution in the case of weak acid sites.

### CONCLUSION

The adsorption of ammonia with subsequent temperature programmed desorption give the possibilities to test the acid sites of dealuminated zeolites. There are two consequences of dealumination:

- i) The EFA1 remained in zeolite structure is the product of izomorphous substitution, increases the weak acid sites determination by  $\text{NH}_3\text{-TPD}$  and is the cause of the shift of A, B-peak position to higher temperature. Acid washing decreases the weak acid sites peak areas and increases the strong ones as the result of EFA1 removing.
- ii) The dissolution-degradation is the by-process of izomorphous substitution, the results of which is mesopore formation and the shift of C, D, E peaks position to lower temperature.

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Submitted in English by the authors

### ŠTÚDIUM TEPLOTNE PROGRAMOVANEJ DESORPCIE $\text{NH}_3$ Z DEALUMINOVANÉHO KLINOPTILOLITU POMOCOU DTG A HMOTNOSTNÝCH SPEKTIER

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Ryolitický tuf s obsahom klinoptilolitu 70% bol dealuminovaný vodným roztokom  $(\text{NH}_4)_2\text{SiF}_6$ .  $\text{NH}_3$  bol adsorbovaný na deamonizovaný a dehydratovaný povrch kalcinovaných vzoriek zeolitu. Metódou teplotne programovanej desorpcie boli rozlíšené 4 typy kyslých centier. Realitný počet kyslých centier je funkciou stupňa dealuminácie a je závislý aj na použití kyslého preplachu dealuminovaných vzoriek. Kyslým preplachom sa odstraňuje mimoštruktúrny hliník, vytvorený dealumináciou, ktorý má blokujúci vplyv na stanovenie počtu silných kyslých centier.

Obr. 1: DTG krivka desorpcie  $\text{NH}_3$  zo vzorky  $D_3$  a fitované desorpčné píky.

Obr. 2: Hmotnostné spektrá desorpcie  $\text{NH}_3$  zo vzorky  $D_3$ .

Obr. 3: Závislosť realitnej plochy píkov desorpcie  $\text{NH}_3$  od stupňa dealuminácie.

Obr. 4: DTG krivky desorpcie  $\text{NH}_3$  pre rôzne stupne dealuminácie.

Obr. 5: Porovnanie výsledkov termickej analýzy vzorky  $\text{NH}_3\text{-D}_0$  vo vzduchu a v dusíku.